SOURCE TEST PLAN 2019 Ethylene Oxide Test Program Medline Industries, Inc. Howell, Michigan

Prepared For:

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For Submittal To:

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Project Overview

General

The procedures outlined in this test protocol cover the air emissions test program to be conducted at the Medline Industries, Inc. (Medline) facility located in Howell, Michigan. The specific objectives of the test program are to:

- Monitor the emissions of ethylene oxide (EtO) from the thermal oxidizer (TO) at the inlet and outlet for three (3) runs during the chamber evacuation cycle
- Monitor the emissions of EtO from the dry beds (DB) at the inlet and outlet for three (3) runs each of one (1) hour duration
- Determine the EtO destruction efficiency of the TO and DB

Testing will be conducted by Montrose Air Quality Services, LLC. (MAQS). Coordinating the test program will be:

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Methodology

EtO Emissions Testing Methodology

The emissions of EtO at the TO and DB locations will be determined using EPA Method 320. In Method 320 a sample of the gas stream will be withdrawn from the test location at a constant rate through a heated Teflon sample line and passed directly into a gas analyzer that utilizes Fourier Transform Infrared (FTIR) spectroscopy.

To convert the EtO concentrations to mass flow rates at the outlet, the volumetric gas flow rate will be determined at each test location using EPA Methods 1 and 2. Due to the ambient nature of the outlet test locations, the carbon dioxide and oxygen concentrations will not be determined and the molecular weight will be assumed to be 29.0 as allowed by EPA Method 2, Section 8.6. The moisture content will be calculated based on the EtO concentrations at the inlet and outlet of the TO and DB.



Parameters

The following gas parameters will be determined at each source test location.

- duct temperature
- moisture concentration
- gas velocity
- EtO concentration

Test Schedule

Testing is currently scheduled for October 23, 2019. Testing will be performed according to the following schedule of activities.

Date	Location	Activity	Test Method
10/22	Howell, MI	Setup test equipment	
10/23	Thermal Oxidizer & Dry Bed sources	Three (3) one (1) hour runs (Dry Bed)	1, 2, 320
		Three (3) chamber evacuation cycles (Thermal Oxidizer)	

Test Procedures

Method Listing

The test methods found in 40 CFR, Part 60, Appendix A will be referenced during the test program. The following individual methods will be referenced:

- Method 1 Sample and Velocity Traverse for Stationary Sources
- Method 2 Determination of Stack Gas Velocity and Volumetric Flow Rate (Type S Pitot Tube)
- Method 320 Method 320 Vapor Phase Organic and Inorganic Emissions by Extractive FTIR

Method Descriptions

Method 1

EPA Method 1 will be used to determine the suitability of the test locations and to determine the traverse points used for the volumetric flow rate determinations. The test locations must conform to the minimum requirement of being at least 2.0 diameters downstream and at least 0.5 diameters upstream from the nearest flow disturbances.

Method 2

EPA Method 2 will be used to determine the gas velocity through each test location using a Type S pitot tube and an incline plane oil manometer. The manometer will be



leveled and "zeroed" prior to each test run. The sample train will be leak checked before and after each run by pressurizing the positive side, or "high" side, of the pitot tube and creating a deflection on the manometer of at least three in. H_2O . The leak check will be considered valid if the manometer remains stable for fifteen (15) seconds. This procedure will be repeated on the negative side by generating a vacuum of at least three in. H_2O . The velocity head pressure and gas temperature will then be determined at each point specified in Method 1. The static pressure of the duct will be measured using a water filled U-tube manometer. In addition, the barometric pressure will be measured and recorded. The Method 2 sampling apparatus is shown in Figure 1 in the Appendix.

Method 320

The EtO concentrations at the TO and DB inlet and outlet test location will be determined using EPA Method 320. In Method 320, a sample of the gas stream will be continuously withdrawn from the test location and analyzed using a continuous FTIR gas analysis system.

The sample gas will be withdrawn from the test location at a constant rate through a stainless-steel probe and a heated Teflon sample line. The sample line will be operated at a temperature of 200°F or greater to prevent the condensation of moisture. The wet gas will then be directed to the FTIR spectrometer gas cell. Results from the analyzer will be determined on a "wet" volume basis.

The FTIR gas analyzer that will be used for this project at the inlets is a MKS MultiGas FTIR analyzer and at outlets is a Max Analytical Starboost FTIR analyzer. A schematic of the sampling system can be found in Figure 2 in the Appendix.

Prior to testing, the detection limit (DL) and analytical uncertainty (AU) will be determined for each constituent. The potential interferants for the analytes being tested will be determined. The optical configuration that can measure all of the analytes within the absorbance range of 0.01 and 1.0 will be determined. The sample system will be assembled and allowed to reach stable operating temperatures and flow rates. A sample interface leak check will be performed. Nitrogen or zero air will be directed to the FTIR gas cell to determine a background spectrum. A sample spectrum will then be recorded in succession. The peak to peak and RMS noise in the resultant spectrum in the wavelength region(s) to be used for the target compound analysis will be measured and recorded.

A Calibration Transfer Standard (CTS) will be introduced into the system and two spectra will be recorded at least two minutes apart. If the second spectrum is no greater than the first and within the uncertainty of the gas standard, it will be used as the CTS spectrum.

A QA spike will be performed by introducing a certified standard of EtO into the sampling system. First, some of the effluent gas will be sampled to determine native concentration of target analytes. The analyte spike calibration gas will then be introduced to the FTIR gas cell only, and the results will be determined using the analytical algorithm. Results from the calibration gas will be recorded and compared to the certified value of the calibration gas. For reactive condensable gases such as hydrogen chloride (HCI), ammonia (NH3), and formaldehyde (HCHO), the results must be within 10% or 5 ppm. For RATA class gases, the FTIR results should be within 2% of



the certified value. The analyte spike calibration gas will then be directed through the entire sampling system and allowed to mix with effluent gas sample at a known flow rate. The flow ratio of calibration gas to ambient air or source effluent shall be no greater than 1:10 (one-part calibration gas to ten parts total flow) for the determination of sample recovery. Spectra will be recorded for three non-consecutive spiked samples and the concentration of the spike will be calculated. The average spiked concentration must be within 70% and 130% of the expected concentration.

After all the required pre-test procedures have been performed, stack gas will be sampled continuously. Sample interferograms, processed absorbance spectra, background interferograms, CTS sample interferograms, and CTS absorbance spectra will be recorded. Sample conditions, instrument settings, and test records will also be recorded throughout the test. If signal transmittance changes by five (5) percent or more in any analytical spectral region, a new background spectrum will be obtained. A new CTS spectrum will be obtained after each sampling run. The post-test CTS spectrum will be compared to the pre-test spectrum. The peak absorbance from each spectrum must be within five (5) percent of the mean value.



Appendix

Figures





Sample Calculations

Area of Sample Location

$$A_s = \pi \times \left(\frac{d_s}{2 \times 12}\right)^2$$

where:

As	= area of sample location (ft ²)
ds	= diameter of sample location (in)
12	= conversion factor (in/ft)
2	= conversion factor (diameter to radius)

Stack Pressure Absolute

$$P_a = P_b + \frac{P_s}{13.6}$$

where:

Pa	= stack pressure absolute (in. Hg)
Pb	= barometric pressure (in. Hg)
Ps	= static pressure (in. H ₂ O)
13.6	= conversion factor (in. H_2O/in Hg)

Molecular Weight of Dry Gas Stream¹

$$M_{d} = \left(44 \times \frac{\% CO_{2}}{100}\right) + \left(32 \times \frac{\% O_{2}}{100}\right) + \left(28 \times \frac{(\% CO + \% N_{2})}{100}\right)$$

Md	= molecular weight of the dry gas stream (lb/lb-mole)
%CO2	= carbon dioxide content of the dry gas stream (%)
44	= molecular weight of carbon dioxide (lb/lb-mole)
%O2	= oxygen content of the dry gas stream (%)
32	= molecular weight of oxygen (lb/lb-mole)
%CO	= carbon monoxide content of the dry gas stream (%)
$%N_2$	= nitrogen content of the dry gas stream (%)
28	= molecular weight of nitrogen (lb/lb-mole)
100	= conversion factor

¹ The remainder of the gas stream after subtracting carbon dioxide and oxygen is assumed to be nitrogen.

Molecular Weight of Wet Gas Stream

$$M_{s} = \left(M_{d} \times \left(1 - \frac{B_{wo}}{100}\right)\right) + \left(18 \times \frac{B_{wo}}{100}\right)$$

where:

Ms

- = molecular weight of the wet gas stream (lb/lb-mole)
- M_d = molecular weight of the dry gas stream (lb/lb-mole)

B_{wo} = moisture content of the gas stream (%)

- 18 = molecular weight of water (lb/lb-mole)
- 100 = conversion factor

Velocity of Gas Stream

$$V_{s} = 85.49 \left(C_{p}\right) \left(\sqrt{\Delta P}\right) \sqrt{\frac{\left(T_{s} + 460\right)}{\left(M_{s}\right) \left(P_{b} + \frac{P_{s}}{13.6}\right)}}$$

where:

Vs	= average velocity of the gas stream (ft/sec)
Cp	= pitot tube coefficient (dimensionless)
√∆P T₀	= average square root of velocity pressures (in. H_2O) ^{1/2}
Ms	= molecular weight of the wet gas stream (lb/lb-mole)
P _b	= barometric pressure (in. Hg)
Ps	= static pressure of gas stream (in. H ₂ O)
85.49	= pitot tube constant (ft/sec)([(lb/lbmole)(in. Hg)]/[(°R)(in. H ₂ O)]) ^{1/2}
460	= conversion (°F to °R)
13.6	= conversion factor (in. $H_2O/in Hg)$

Volumetric Flow of Gas Stream - Actual Conditions

$$Q_a = 60(V_s)(A_s)$$

- Q_a = volumetric flow rate of the gas stream at actual conditions (acfm)
- V_s = average velocity of the gas stream (ft/sec)
- A_s = area of duct or stack (ft²)
- 60 = conversion factor (sec/min)

Volumetric Flow of Gas Stream - Standard Conditions

$$Q_{std} = \frac{17.64(Q_a)\left(P_b + \frac{P_s}{13.6}\right)}{(T_s + 460)}$$

where:

Qstd	= volumetric flow rate of the gas stream at standard conditions
(scfm)	
Qa	= volumetric flow rate of the gas stream at actual conditions (acfm)
Ts	= average stack temperature (°F)
Pb	= barometric pressure (in. Hg)
Ps	= static pressure of gas stream (in. H ₂ O)
13.6	= conversion factor (in. H ₂ O/in Hg)
17.64	= ratio of standard temperature over standard pressure (°R/in.Hg)
460	= conversion (°F to °R)

Volumetric Flow of Gas Stream - Standard Conditions - Dry Basis

$$Q_{dstd} = Q_{std} \left(1 - \frac{B_{wo}}{100} \right)$$

Qdstd	= volumetric flow rate of the gas stream at standard conditions, on
	a dry basis (dscim)
Q _{std}	 volumetric flow rate of the gas stream at standard conditions (scfm)
Bwo	= moisture content of the gas stream (%)
100	= conversion factor

Ethylene Oxide Emission Rate (lb/hr)

$$E_{lb/hr} = \frac{(C_w)(MW)(Q_{dstd})(60)}{385.3 \times 10^6}$$

Elb/hr	= EtO emission rate (lb/hr)
Cw	= EtO concentration (ppmdv)
MW	= molecular weight of EtO (lb/lbmole)
60	= conversion factor (min/hr)
385.3	= volume occupied by one pound of gas at standard conditions (scf/lbmole)
10 ⁶	e conversion factor (fraction to ppm)

Field Work Safety Plan



Site Safety Plan Booklet

Finalized: April, 2018

Introduction

Employee safety is the top priority of Montrose Environmental Group. All employees must be trained to mitigate the hazards faced each day. The site manager and project manager/lead are responsible to ensure all hazards have been proper identified and managed. All employees have Stop Work Authority in all situations where an employee feels they cannot perform a job safely or a task for which they have not been adequately trained.

The Site Safety Plan (SSP) has been developed to help assist Montrose test crews with identifying physical and health hazards that could harm our employees and determining how the hazards will be managed. Additionally, the SSP will help each crew manage the health of the employees by providing emergency procedures and information.

The booklet contains all the different safety forms that you may need in the field into one document. The SSP consists of the following:

- 1. A standardized, two-page, fillable pdf, form that is used as the Hazard Analysis and Safety Plan
- 2. Hazard Control Matrix contains useful information on both engineering and administrative controls that a crew can use to reduce or eliminate the hazards they have observed plus applicable PPE that may be required
- 3. Tool Box Meeting Record Keeps a daily record of the scheduled testing for the day and a short refresher of the hazards that were identified in the test location SSP and any hazard controls/PPE
- 4. Additional Forms
 - a. Aerial Lift Inspection Form
 - b. Heat Stress Prevention Form
 - c. Extended Hours Form
 - d. Safe Work Permit

An SSP for each location must be completed or at least started prior to mobilization and included as part of your Project Test Plan. Each test crew will then assess the hazards again while on-site looking for changes or new hazards. Once an SSP is completed, it will need to be reviewed before set up at each of your client's testing locations. Any day a SSP is not reviewed, a Tool Box Meeting will need to be completed.

The SSP is a living document. Each test crew should update the plan as new hazards are found. The client project manager should continually update their SSPs as new information and conditions result in new or changed hazards. The goal is to provide each crew with the most upto-date hazard and safety information

MAQS Site Safety Plan

Client			Contact Name		C	Date
Location			SSP Writer		F	M
Job Prepa	ration					
Job S	ite Walk Through Co	ompleted Site	Specific Training C	omplete C	ertified First Aid Pers	on
Site V	Valk Through Neede	d Site	Specific Training N	eeded C	other:	
Facility Inf	ormation/Emergen	cy Preparedness				
Plant Em	ergency #		Identify a	nd Locate the	following:	
On-Site F	EMS Yes	No	Evacua	tion Routes	0	
FMS L oc	ation		Severe	Weather She	ter	
Nearest			Rally P	oint		
Nouroot	orgonic ouro r donity.	·	Locatio	n of Eve Wast	Safety Shower	
					"ealery enemen	
Source Inf	ormation (list type)	•				
Flue Gas	s Temp (°F)	Elue Gas Press	("H O) Eli	le Gas Compo	nente:	
	Inholotion Dotontia		(H ₂ O) H			
Flue Gas		l res	NO			
Describe	Hazard Protection					
Required F	PE Hard Hat	ts Safety Glas	sses Steel To	ed Boots	Hearing Protection	
Addition	al PPE Requirement	nts				
Hi-Vis	s Vests	Harness/Lanyard*	Goggles	Persor	al Monitor Type:	
Metat	arsal Guards	SRL(s)	Face Shield	Respir	ator Type:	
Nome	x/FRC	Hot Gloves	4-Gas Moni	tor Other I	PPE:	
Critical Pro	ocedures – check a	ll that apply – "*" i	ndicates additiona	l form must b	e completed	
Hot W	/eather Work*	Confined Space*	Aerial Wo	ork Platform*	Roof Work	Scaffold
Cold \	Weather Work	Lock out/Tag Ou	t Exposure	Monitoring	Other:	
Working a	at Heights Manag	ement				
Fall Protec	tion Plan Fixed	d Guardrails/Toeboa	ards Fall Pro	otection PPE	Warning Line	•
Describe	Hazard Protection	Plan:			· ·	
Falling Ob	iects Protection Pl	an				
Barrice	adina Nettina	House Keening	Tethered Tool	Catch	Blanket or Tarn	Safety Spotter
Describe	Hazard Protection [Dian.		Gaton		Ouldry Opener
Describe		iaii.				

MAQS Site Safety Plan

Fall Hazard Communi	cation Plan						
Adjacent/Overhead Work		Contractor Contact Client Con		Client Con	tact		
Describe Communic	ation Plan:						
Environmental Hazard	ds - Weather Forecas	st					
Heat/Cold	Lightning F	Rain Sr	NOW	Ice 7	Fornado	Wind Speed	
Describe Hazard Pro	tection Plan:						
Additional Work Pla	ICE Mazaros	ntrolo					
Physical Hazards		ntrois	Other				
Thermel Burn	Zaros Dust Mask	Goggies	Uther:	r Drotactiva (Nothing		
Electrical Hozarda			n Elemente	Evtornal		thor	
		no rany Lighting				inei.	
Slin and Trin	Housekee		de Area	Autamps Other			
Describe Hazard Pro	I lousekee	bing Damea	ue Alea	Ouner			
List of Hazardous Ch	emicals				Other Che	emicals:	
Acetone Nitr	ic Acid Hyd	drogen Peroxide	Compress	ed Gases	•		
Hexane Sul ¹	furic Acid Iso	propyl Alcohol	Flamma	able Gas			
Toluene Hyd	Irochloric Acid Liq	uid Nitrogen	Non-Fla	ammable Gas	3		
Describe Hazard Pro	tection Plan:	C					
Wildlife/Fauna							
Describe Hazard Pro	tection Plan:						
Crew Names & Signat	tures						
Print Name	Signature	Date	Prir	it Name		Signature	Date
	· · · · ·					-	

Job Site Hazard Mitigation Plan

Hazard	Description	Engineering Controls	Administrative Controls	PPE
Ergonomic: Strains/Sprains	The manual movement of equipment to testing location can cause strains	 Eliminate manual "lifts" and use elevators and/or cranes when possible. Stairs can also be used where feasible. Use lifting straps and locking carabiners to eliminate the need to continuously tie and untie loads. Use pulley system to eliminate improper ergonomics when lifting and facilitate sharing of loads Winches should be evaluated and used as much as possible to assist Equipment should be staged on table or other elevated platform to assist with rigging, lifting and prevent bending over when securing equipment to hoist. Maintain radio contact between ground and platform to ensure the process is going smoothly or if a break is needed. 	 Stretching prior to and after lifting and lowering tasks to keep muscles and joints loose Break loads into smaller more manageable portions 3 man lift teams during initial set up and tear down w/2 below and one above Job rotation and/or breaks during initial set up and tear down. Discuss potential hazard and controls during tailboard meetings Observe others and comment on technique 	Gloves, appropriate to task
Falling objects	When working from heights there is a potential of falling objects from elevated work platform striking someone or something below	 Ensure job area is barricaded off with hazard cones, caution tape and/or appropriate warning signs. Specific measures should comply with local plant rules. Ensure a spotter is present during a lift or lowering of equipment. Catch blanket should be used on the platform to prevent objects from falling through any grating. Magnetic trays should be used to hold flange bots and nuts. Tools should be tethered to platform or personnel uniform. 	 Review hazards with any adjacent workers & the client so they understand the scope and timing of the job Follow proper housekeeping practices by keeping the test location neat and orderly, keeping trash in bags and non-essential equipment stored when not in use. Perform periodic job site inspections to ensure housekeeping is being observed Review "grab and twist" method of handling tools and equipment between employees 	 Hardhat Steel toed boots Work clothes

Job Site Hazard Mitigation Plan

Hazard	Description	Engineering Controls	Administrative Controls	PPE
Fall	Fall hazard exists when working from above 4' with no guardrails	 Verify anchor point Warning Line system 	 Review Working from Heights procedure prior to job Maintain 3 points of contact when climbing stairs or ladders Ensure all fall protection equipment has been inspected and is in good working order 	• Harness and Lanyard
Burn	Flue gas temperature can be elevated and that can lead to hot temperature testing equipment. Hot pipes or other duct work at plant.	 Use heat resistant refractory blanket insulation to seal port once probe is inserted. Use duct tape to further seal the outer flange area of the port. Use heat resistant blankets to shield workers from hot sources 	 Work in tandem with partner to immediately fill sample port with heat resistant refractory insulation Stand up wind of port when opening. If stack pressure is greater than 2" H₂O, a face shield is required. Allow appropriate time to handle probes Notify all team members at the test location when a probe is removed from a hot source and communicate to all crew members to exercise caution handling or working near the probe 	 High temp. gloves Long gauntlets Long sleeve shirts FRC
Atmosphere	Air concentrations could be above PEL	 Probe are to be sealed to prevent stack gases from leaking out Ventilation, open all doors and window to dilute concentrations in work area Vent analyzer or meter outside 	 Stand up wind of ports Use a gas monitor to ensure levels of contaminants are below PEL 	RespiratorSAR
Hearing	Production areas of plants could be high	NA	 Set up equipment or trailer as far away as possible from noise producing plant equipment. 	 Ear plugs Ear muffs (check with plant contact on exposure levels)

Hazard	Description	Engineering Controls	Administrative Controls	PPE
Fire	High flue gas temps, chemicals, electricity could cause fire	• Fire extinguisher at job location	 Observe proper housekeeping If conducting hot work, review procedures and permitting with site contact 	• N/A
Weather	Conditions may pose significant hazards	 Weather App warning 	 Lightning policy JHA review of weather daily Plant severe weather warning systems 	 Appropriate clothing for conditions
Hot Weather	Extreme hot temperatures can cause physical symptoms	 Shade Reduce radiant heat from hot sources Ventilation fans 	 Frequent breaks Additional water or electrolyte replenishment Heat Stress Prevention Form Communication with workers Share work load 	 Appropriate clothing for conditions Sunscreen
Cold Weather	Extreme cold temperatures can cause physical symptoms	Hand warmersHeatersWind blocks	 Calculate wind chill Frequent warm up periods Communication with workers 	 Appropriate clothing for conditions
AWP	Overhead and ground hazards pose dangers	 Ensure all fall protection equipment has been inspected and is in good working order Barricade off area where AWP is in use 	 AWP pre-use inspection can identify problems with equipment Site walk through can identify overhead and ground hazards 	 Hardhat Steel toed boots Safety glasses Harness/lanyard Gloves
Scaffold	Fall hazard	 Yellow tagged scaffold may require harness & lanyard Inspect harness & lanyard prior to use Barricades Netting 	 Scaffold inspection prior to use can identify if scaffold meets OSHA regulations Current scaffold training 	 Hardhat Steel toed boots Safety glasses Harness/lanyard

Job Site Hazard Mitigation Plan

Hazard	Description	Engineering Controls	Administrative Controls	PPE
Chemicals	Chemical fumes	Chemical containers stored properly	Spill kit training	 Safety glasses
	or splashing can	Ventilation	• Lab SOP	Chemical gloves
	cause asphyviation or	Properly labeled secondary containers	Good housekeeping	Lab coat
	burns		Personal nyglene	
				 Goggles/Face shield as needed

Daily Tool Box Meeting Record

lien <u>t:</u>	Job I	No.:	Location:			Date:
cope of	Work:					
hanges	<u>in Hazards</u> Any sig	gnificant change in Hazard	s, update Site Specific Pla	an and sign off.		
ite Spec	ific Plan review					
	Emergency Preparatior	Rally Point	Alternate Exits	Obstacle	es in Route	
	Source	Stack Temp.	Static Pressure	Flue gas	contaminants	
	PPE	Hard Hats Sa Hi-Vis Vests Ha Metatarsals Sf Nomex/FRC Ho	afety Glasses Ste arness* Gog RL Face ot Gloves 4-Ga	el Toed Boots gles e Shield as Monitor	Hearing Protec Personal Monite Respirator Type Other PPE:	tion pr Type: ::
	Critical Procedures	Scaffold LOTO	Aerial Work Plat	.form*	Confined Space*	
	Fall Protection	Guardrails	Fall Protection		Warning Lines	
	Working at Heights	Barricading Housekeeping	Tethered Tools Catch Blanket	_	Netting Other:	
	Barricades Mornin	g Inspection	inted Namo		Sig	actura
		PII			Sigi	lature
	EOBD	Inspection Pri	inted Name		Sigi	nature
	Communication	Adjacent/Overl	head Work	Contractor Cor	ntactClie	nt Contact
	Weather	Forecast Temperature Fluids Reminde	Lightning Cold er Proper Clo		Wind Speed Hot*, <i>above 91°F use H</i> Ice-Rain	_ Wind Direction eat Stress Prevention Form Snowy
	Workplace Hazards	Dust	Electrical Slips	s, Trips & Falls	 Thermal Burn	 Lighting
	Chemical	Labeling Storage	PPE Ventilation	Cylinders	s Secured Storage	0 0
	Surroundings	Site Traffic Construction Machine Guard	Trucks Cranes ding Chemical	Fo Wi Up	rklifts ildlife/Fauna wind/downwind Hazards	
	Harness & Lanyard	Inspected by:				
		Printed Name		Siç	gnature	
		Printed Name		Siç	gnature	
		Printed Name		Siç	gnature	
aal Dave '	Maating Loads - Circature				Test Crew Initials:	
OOI ROX I	weeting Leader Signature					
otes:						

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Montrose Air Quality Services -Daily Aerial Lift Inspection Form

All checks must be completed before operation of the aerial lift. This checklist must be used at the beginning of each shift or after six to eight hours of use.

General Information (Check All That Apply)

Manually Propelled Lift:	Self-Propelled Lift:
Aerial Lift Model Number:	Serial Number:
Make:	Rented Or Owned?

Initial Description – Indicate by checking "Yes" that an item is adequate, operational, and safe. Check "No" to indicate that a repair or other corrective action is required prior to use. Check "N/A" to indicate "Not Applicable."

Number Item to be Inspected	Yes	Νο	N/A
A. Perform a visual inspection of all aerial lift components, i.e. missing parts, torn or loose hoses, hydraulic fluid leaks, etc. Replace as necessary			
B. Check the hydraulic fluid level with the platform fully lowered			
C. Check the tires for damage. Check wheel lug nuts for tightness			
D. Check the hoses and the cables for worn areas or or chafing.			
E. Check for cracked welds			
F. Check the platform rails and safety gate for damage			
G. Check for bent or broken structural members			
H. Check the pivot pins for security			
I. Check that all warning and instructional labels are legible and secure			
J. Inspect the platform control. Ensure the load capacity is clearly marked			



Initial Description – Continued Number Item to be Inspected	Yes	Νο	N/A
K. Check for slippery conditions on the platform			
L. Verify that the Manufacturer's Instruction Manual is present inside the bucket			
M. Check the hydraulic system pressure (See manufacturer's specifications). If the pressure is low, determine the reason and repair in accordance with accepted procedures as outlined in the service manual			
N. Check the base controls for proper operation. Check switches and push buttons for proper operation			
O. Check the platform controls for proper operation. Check all switches and push buttons, as well as ensuring that the drive controller returns to neutral			
P. Verify that a fire extinguisher is present, mounted, and fully charged and operational inside the bucket			
Q. Verify that the aerial lift has headlights and a safety strobe-light installed and fully operational			
R. Verify that the aerial lift has a fully functional back-up alarm			

Print Name of Individual Inspecting Aerial Location Date Lift

Location

Date

Heat Stress Prevention Form

This form is to be used when the Expected Heat Index is above 91 degrees F. Keep the form with project documentation.

Project Location:		
Date:	Project Manager:	

Expected High Temp:_____Expected High Heat Index:_____

- 1. Review the signs of Heat Exhaustion and Heat Stroke
- 2. If Heat Index is above 91 degrees F:
 - a. Provide cold water and/or sports drinks to all field staff. Avoid caffeinated drinks and energy drinks which actually increase core temperature. Bring no less than one gallon of water per employee.
 - b. If employee are dehydrated, on blood pressure medication or not acclimated, ensure they are aware of heightened risk for heat illness.
 - c. Provide cool head bands, vests, etc.
 - d. Have ice available to employees.
 - e. Encourage work rotation and breaks, particularly for employees working in direct sunlight.
 - f. Provide as much shade at the jobsite as possible, including tarps, tents or other acceptable temporary structures.
 - g. PM should interview each field staff periodically to look for signs of heat illness.
- 3. If Heat Index is above 103 degrees F:
 - a. Employees must stop for drinks and breaks every hour (about 4 cups/hour).
 - b. Employees are not permitted to work alone for more than one hour at a time without a break with shade and drinks.
 - c. Employees should wear cool bands and vests if working outside more than one hour at a time.
 - d. PM should interview each field staff every 2 hours to look for signs of heat illness.





Montrose Air Quality Services

Extended Hours Safety Audit

Project Number: _____ Date: ____ Time: _____

Whenever a project is going to extend past a 14-hourwork day, an Extended Hours Safety Audit to access the condition of their crew and the safety of their work environment must be completed. If a senior tech or a FPM is leading a project, they should confer with the CPM but they will need to get permission to proceed from the DM or RVP. CPMs need to get permission to proceed from the DM or RVP. Technical RVPs can authorize moving forward if they are in the field or if they own the project. DMs and RVPs may make the call in the field.

Hold test crew meeting. Test Crew Initials:

"Extended or unusual work shifts may be more stressful physically, mentally and emotionally. Non-traditional shifts and extended work hours may disrupt the body's regular schedule, leading to increased risk of operator error, injuries and/or accidents."

The test leader should look for signs of the following in their crews:

- Irritability
- Lack of motivation
- Headaches
- Giddiness

• Depression

Fatigue

• Reduced alertness, lack of concentration and memory

The test leader should assess the environmental and hazardous concerns:

- Temperature and weather
- Hoisting

- Lighting
- Climbing

- PPE (respirators, ect.)
- Pollutant concentration in ambient air (SO₂, H₂S, ect.)

Notify DM or RVP Name:

The test leader must contact either the DM or RVP to discuss the safety issues that may arise due to the extended work period. During this time, they can come to an agreement on how to proceed.

Things to discuss are why the long hours? Client or our delays? Production limitations? Impending Weather?

Contact client

The test leader, DM or RVP should discuss with client any of our safety concerns, the client's needs and come to agreement on how to proceed. Discussion should also include the appropriate rest period needed before the next day's work can begin. The DM and/or a RVP must be kept in the loop on what the final decision is.

What was the outcome?



SAFE WORK PERMIT

A. WORK SCOPE (to be completed by MEG) – Check relevant box(es) to indicate type(s) of work.								
Hot Work	Line Break	Lock-out Tag-out	🗆 Other		Permit	Permit Timing		
Specific					Data	Timo:		
Location:					Date.	nine.		
Equipment					Valid	Until		
Worked On:					Vallu	Until		
Work to be					Data	Time		
Performed:					Date:	nme:		

B. POTENTIAL HAZARDS (To be completed by MEG)							
🗆 Flammable	🗆 Harmful	to breathe	Harmful by Skin Cont	act			
Verify process hazards have been been been been been been been be	en reviewed						
C. PERSONAL PROTECTIVE EQUIP	MENT (Chec	k all additional equipme	ent that is required)				
o Tyvek Suit	 Hearing 	Protection	 H2S Monitor 		 Flash Hood 		
o Rain Gear	o Goggles		 Safety Harness & Life 	e Line	o Life Vest		
 Chemical Resistant Gloves 	o Face shi	eld	 Tripod ER Escape Un 	it	 Supplied Air Respirator 		
 Rubber Boots 	o Organic	Vapor Respirator	 Fall Protection Equip 	ment	 Dust Respirator 		
o Other:							
D. CHECK LIST (Check what has be	een complete	ed)					
 Joint Job Site Visit 	o Electrica	I Isolation Completed	 Line Identified 		 Equipment Water Flushed 		
 Equipment Depressurized 	o Isolated	and locked out	 Equipment Identified 	ł	 Equipment Inert Gas Purged 		
 Vents Opened & Cleared 	o Blinds in	Place	 Electrical Equipment 	Still Live	 Written JSA Completed 		
 Atmosphere Tested 	 Electrica 	l Equipment Still Live	 Equipment Still Live 		0		
Other:							
E. PRECAUTIONS (Check what mu	E. PRECAUTIONS (Check what must be completed PRIOR to commencing work)						
• Cover Sewers • Scaffoldi		ing Inspection Done	 Charged Hose/Area 	Wet	 Communication Device(s) 		
• Air Mover (Grounded) • Fire Extin		nguisher	 Covered Cable Trays 		o Fire Watch		
o Barricade/Signs o Fire Resi		istant Blanket	 Continuous Air Monitoring 				
o Other:							
 Designated Fire Watch Individu 	al and Start t	ime (30 min after hot w	ork):				
 Fire Watch Complete (signature 	e and time):						
F. HAZARD ANALYSIS (add additio	onal informat	tion to form as necessar	γ)				
Job Steps		Potential Hazards		Hazard C	ontrols		
1.							
2.							
3.							
4.							
I VERIFY THAT THE ABOVE CHECK MET, THE AREA IS SAFE FOR WOR	LIST "D" HAS K TO COMMI	BEEN COMPLETED, ALL ENCE.	OTHER CONDITIONS ("B'	", "C", "E",	"F") ARE UNDERSTOOD AND WHEN		
Name:	Signature:		Date:		Time:		

Example Data Sheets

MONTROSE AIR QUALITY SERVICES, LLC

EPA Method 1 Sample and Velocity Traverses Datasheet

LOCATION



Location Schematic and Notes	Point	
		(in.)
	1	
	2	
	3	
	4	
	5	
	6	
	7	
	8	
	9	
	10	
	11	
	12	
	13	
	14	
Indicate sample ports, height from grade, types of disturbances, access, unistrut configuration, etc.	15	
Distance to point must include length of port	16	

MONTROSE AIR QUALITY SERVICES, LLC

EPA Method 2

Cyclonic Flow Traverse Datasheet

Client			
Project No.			
Plant			
Location		Duct size (in)	
Date		Port Length (in)	
Probe ID		Pitot Cp	

	Page		of				
▲							
(N 1761 I 1							
[N][Up]							
F	irst point all th	he way [in] [o	ut]				
	Gas flow [in] c	or [out] of pag	<i>j</i> e				
Cross Section of Duct							

Run Number		Run Numb		ber			Run Number				
Start Time				Start Time				Start Time			
Stop Time				Stop Time				Stop Time			
Barometric (inHa)				Barometric (inHg)				Barometric (inHa)			
Static (in	H₂O)			Static (inH ₂ O)				Static (inH ₂ O)			
Probe Op	erator			Probe Operator				Probe Operator			
Data Reco	order			Data Recorder				Data Recorder			
Pre Leak	Check			Pre Leak Check				Pre Leak Check			
Post Leak	Check			Post Leak Check				Post Leak Check			
	Pressure	Angle		Pressure		Angle		Pressure		Angle	
Traverse Point	∆P @ 0 ⁰ (in H₂O)	α (< 20 ⁰)	Notes	Traverse Point	∆P @ 0 ⁰ (in H₂O)	α (< 20 ⁰)	Notes	Traverse Point	∆P @ 0 ⁰ (in H₂O)	α (< 20 ⁰)	Notes
	、 <u>-</u> /				、 <i>_</i> ,				、 _ ,		
Total				Total				Total			
Average				Average				Average			

EPA Methods 2 and 4

Velocity and Moisture Datasheet

RUN NO.

Total Average

Client		
Project No.		
Plant		
Location	Dat	te
Meter Operator		
Probe Operator		

Meter Ope	erator										
Probe Ope	erator										
									[N]	[Up]	
			EPA Meth	hod 4						First point all the way [in] [out]	
Meter ID			Yd		F	Pitot	Ср		Gas flow [in] [out] of page		
Pre-Test L	.eak Check	(cfm @		(in. Hg)			Cross Section of Duct		
Post-Test	Leak Chec	k		cfm @			(in. Hg)				
Start Time)			Stop Time							
Water [ml]	I			Silica gel ((g)						
-								-			
Min/Point Elapsed Time	Orifice Setting ∆H (inH₂O)	Gas V Ini	s Sample olume itial [ft]	Impinger Outlet Temp (⁰ F)	DGI Inle Terr (⁰F	M et np)	DGM Outlet Temp (⁰ F)	Pu Vac (in	mp uum Hg)	Notes	

		EPA	Method 2				
Barometric	(inHg)		Probe ID				
Static (inH ₂	2 O)		Duct Dim.	Duct Dim. (in)			
Ambient Te	Ambient Temp (⁰F)		Port Lengt	h (in.)			
Run Numb	er		Run Numb	er			
Start Time			Start Time				
Stop Time			Stop Time	Stop Time			
Pre Leak C	heck		Pre Leak C	Pre Leak Check			
Post Leak	Check		Post Leak	Post Leak Check			
	Velocity			Velocity			
	Pressure	Stack		Pressure	Stack		
Points	ΔP	Temp	Points	ΔP	Temp		
	(in H ₂ O)	(⁰F)		(in H ₂ O)	(⁰F)		
Total			Total				
Average ∆P			Average ΔP				
Ave. Stack 7	Temp.		Ave, Stack '	Ave Stack Temn			

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